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(54) Title: POLYALKYLALUMINOXANE COMPOSITIONS FORMED BY NON-HYDROLYTIC MEANS (57) Abstract The present invention relates to a process which comprises the non-hydrolytic transformation of an aluminosilicate precursor composition, comprising carbon-to-oxygen bonds which can be alkylated by the alkylaluminum moiety, into a catalytically useful aluminosilicate composition. In one embodiment of this invention, the catalytically useful aluminosilicate composition is a polymethylaluminosilicate composition substantially free of trimethylaluminum. The intermediate precursor is formed by the reaction of a trialkylaluminum compound, or a mixture of trialkylaluminum compounds, and a compound containing a carbon-to-oxygen bond, such as an alcohol, ketone, carboxylic acid, or carbon dioxide. Either unsupported or supported polymethylaluminosilicate compositions can be formed.		

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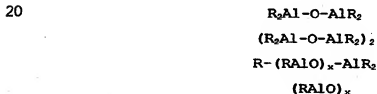
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POLYALKYLALUMINOXANE COMPOSITIONS
FORMED BY NON-HYDROLYTIC MEANS

5 Background of the Invention

10 The present invention relates to a novel synthesis of aluminoxanes by non-hydrolytic means and to novel aluminoxane compositions. Aluminoxanes are well known as components for olefin polymerization catalysts.

Aluminoxane compounds are chemical species that incorporate Al-O-Al moieties. While a wide range of 15 aluminoxane species are known, their exact structures are not precisely known. The following structures (where R is alkyl and X is an integer of from about 1 to about 40) have been depicted:



25 Cyclic and cage cluster structures have also been proposed. Such materials, as would be recognized by the person of ordinary skill in the art are complex mixtures of various species which can easily undergo dynamic exchange reactions and structural rearrangements. A 30 recent review of these materials was authored by S. Pasynkiewicz and appears in Polyhedron, Vol. 9, pp. 429-453 (1990).

Methylaluminoxanes, sometimes termed "polymethylalumin-oxanes" (PMAOs) are well known materials 35 with wide utility in olefin polymerization using single-

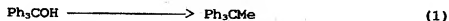
site, or metallocene-based, polymerization catalyst systems (See, for example, Col. 1, lines 14-29 of U.S. Patent No. 4,960,878 to C. C. Crapo et al.). PMAOs are conventionally prepared by controlled hydrolysis of trimethylaluminum (TMAL). Generally, hydrolysis occurs with some loss of aluminum to insoluble species. Generally, PMAOs also have very low solubility in aliphatic solvents, which limits their utility, as well as poor storage stability for solutions containing them.

(See, for example, Col. 1, lines 30-46 of U.S. Patent No. 4,960,878). Finally, it is generally polymethylaluminumoxanes that have been the most useful products of this general class of material: other alkylaluminumoxanes do not work as well. Since TMAL is an expensive starting material, the resulting PMAO is expensive.

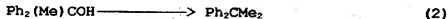
The problems of low yield, poor solubility, poor storage stability, and expensive reagents in preparation of PMAO have previously been attacked, with only limited success, in several ways. One method was to make predominantly PMAO, but include some components from hydrolysis of other aluminum alkyls, to form the so-called "modified methylaluminumoxane" (MMAO). This yields predominantly methyl-containing aluminumoxanes in improved yields, with improved solution storage stability as well as improved solubility in aliphatic solvents, at lower cost. However, since alkyl groups other than methyl are present, these materials are not always as effective as conventional PMAO.

The prior art contains certain disclosures which are deemed to be particularly germane to the present invention, including a series of related publications by

T. Mole and coworkers (E. A. Jeffrey et al., Aust. J. Chem. 1970, 23, 715-724; A. Meisters et al., Journal of the Chemical Society, Chem. Comm. 1972, 595-596; D. W. Harney et al., Aust. J. Chem. 1974, 27, 1639-1653; A. Meisters et al., Aust. J. Chem. 1974, 27, 1655-1663; and A. Meisters et al., Aust. J. Chem. 1974, 27, 1665-1672) which describe the exhaustive methylation of oxygen-containing organic substrates by trimethylaluminum (hereinafter abbreviated as "TMAL" for simplicity). Some of the reactions that these publications report are listed hereinbelow:



Excess TMAL, 19 hrs., 80 °C



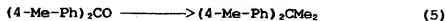
Excess TMAL, 20 hrs., 85 °C



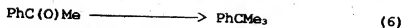
Excess TMAL, 18 hrs., 110 °C



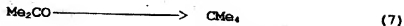
Excess TMAL, 42 hrs., 120 °C



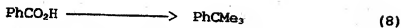
Excess TMAL, trace benzoic acid,
2 hrs., 170 °C



Excess TMAL, 65 hrs., 122 °C



Excess TMAL, 80 hrs., 175 °C



Excess TMAL, 24 hrs., 130-150 °C



15 Excess TMAL, 23 hrs., 130 °C

20 This work focused on conversion of the organic
substrates, and only speculates occasionally on the aluminum
containing products formed. Some of the comments they do make
include, e.g., Equation (6) of Meisters et al. (Aust. J. Chem.
20 1974, 27, 1655-1663) which shows $[\text{Me}_2\text{AlOAlMe}_2]$ as a speculative
product; as well as Equation (6) of Meisters et al. (Aust. J.
Chem. 1974, 27, 1665-1672) which also shows $[\text{Me}_2\text{AlOAlMe}_2]$ as a
speculative product. Another relevant comment made in these
disclosures is that these reactions do not remain homogeneous
25 (see the footnote on page 1643 of Harney et. al, Aust. J.
Chem. 1974, 27, 1639-1653).

Another relevant comment appears in Comprehensive Organometallic Chemistry II, E.W. Abel et al., eds., New York NY, Pergamon, 1995, Vol. 1, p. 452 where several preparations of aluminoxanes are given, including those set forth in Equations (54)-(57) and Scheme 8. Aluminoxanes of these preparative methods, however, are said to be unsuitable as cocatalysts for single-site catalysts.

Another problem well known in the art is the inevitable presence of trimethylaluminum (TMAL) in the polymethyl-aluminoxane (PMAO) product. In particular, L. Resconi et al, Macromol. 1990, 23, 4489-4491 and the references cited therein show that PMAO prepared in the normal manner contains both methylaluminoxane species as well TMAL species. These researchers based their conclusion on, among other things, the presence of two signals in the ^1H NMR of PMAO. Fig. 1, which forms a part of the present specification, illustrates the ^1H NMR of commercially available PMAO with the spectrum being composed of both a broad peak, attributed to methylaluminoxane species, and a distinct second peak, attributed to trimethylaluminum species. M.S. Howie, "Methylaluminoxane and Other Aluminoxanes-Synthesis, Characterization and Production", Proceedings, MetCon '93, pp. 245-266, Catalyst Consultants Inc., Houston, TX 1993, has also noted that PMAO invariably contains TMAL. For instance, on page 247 it is stated that "MAO always contains some amount of TMA". Further, Howie notes that "total removal of TMA from MAO has not been demonstrated, and reduction to low levels creates other problems".

Summary of the Invention

5

The present invention, in one embodiment, relates to a novel composition which is a catalytically useful composition comprising alkylaluminumoxane which is substantially free of trialkylaluminum content. The ^1H NMR of the product of this invention, for example, does not separately distinguish TMAL as a species which is present therein.

This invention also relates to a process for forming aluminosilicates from a particular type of aluminosilicate precursor composition, which will be described in greater detail below, using non-hydrolytic means (e.g., by thermal and/or catalytic means). The intermediate aluminosilicate precursor composition, which is ultimately capable of being transformed by the aforementioned non-hydrolytic means to the desired aluminosilicate product, is formed by treating a trialkylaluminum compound, or mixtures thereof, with a reagent that contains a carbon-oxygen bond. This treatment to form the intermediate aluminosilicate precursor composition is followed by the aforementioned non-hydrolytic transformation of the intermediate aluminosilicate precursor composition to give a catalytically useful aluminosilicate composition. It should be clearly understood that the process described herein can be used to form the novel type of alkylaluminumoxane referred to in the first paragraph of this section of the specification as well as conventional polymethylaluminumoxane compositions that are

not substantially free of TMAL as a species which is present therein as measured by the ^1H NMR spectrum of the product. It should also be recognized that the process described herein is useful for the formation of

- 5 alkylaluminoxanes, in general, as well as the formation of polymethylaluminoxane. In most cases it may be desirable to obtain a polymethylaluminoxane product with a low free TMAL content. However, the amount of free TMAL remaining in the aluminoxane composition may be adjusted from very
10 low levels to over 50% by controlling the stoichiometry and reaction conditions in the process.

- The present invention, in a preferred embodiment, enables one to produce polymethylaluminoxane compositions of improved solution stability which also have the
15 desirable feature of compatibility with aliphatic hydrocarbon solvents, such as hexane, heptane, octane or decane. The process allows for high recoveries (yields) of aluminum values in making the desired product. Also, the process produces an methylaluminoxane product giving
20 high activities in polymerization of olefin monomer(s).

Description of the Drawings

- The Drawings which form a portion of this
25 Specification are provided herewith to further illustrate certain attributes of the present invention. Fig. 1 illustrates the ^1H NMR of commercially available PMAO with the spectrum being composed of both a broad peak, attributed to methylaluminoxane species, and a distinct
30 second peak, attributed to trimethylaluminum species. Fig. 2 shows a novel PMAO product that can be made, in accordance with one particular embodiment of the process

of the present invention, which is easily handled and which performs well, but which is substantially free of TML as a species that can be separately distinguished by ^1H NMR.

5

Description of Preferred Embodiments

10

As just mentioned, preferred embodiments of the present invention relate to (1) a process for forming, by the non-hydrolytic conversion of suitably constituted alkylaluminum precursor compositions, catalytically useful methylaluminum compositions, and (2) polymethylaluminum compositions which are substantially free of trimethylaluminum content and which are catalytically useful methylaluminum compositions.

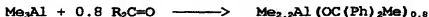
20 The intermediate precursor composition is an organoaluminum composition which is constituted such that it contains alkyl groups, initially bound to aluminum which are capable of alkylation of groups, also contained in the precursor, which contain a carbon-to-oxygen bond.

25 When the alkylation of such carbon-oxygen containing groups occurs, the oxygen atoms contained in such groups in the precursor are incorporated into alkylaluminum moieties during that part of the present process in which the intermediate precursor is transformed to the desired

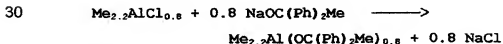
30 aluminosilicate product.

It will be appreciated by a person of ordinary skill in the art that there are many ways of forming the

- intermediate precursor composition which must contain some amount of alkylaluminum groups as well as some carbon which is chemically bound to oxygen and susceptible to alkylation by an alkylaluminum group. For the purposes of
- 5 illustrating the nature of these precursor compositions, the following discussion will provide examples of methods for forming suitable compositions of that type. This discussion, however, should not be construed as limiting the present invention to the particular methods which may
- 10 be exemplified herein, for example, for preparing the preferred aluminosilane precursor composition, which may incorporate a wide range of chemical species therein without precisely known chemical structure. For instance, as will become apparent from the following description, if
- 15 a ketone, such as benzophenone, is reacted with a trialkylaluminum compound, such as trimethylaluminum, an addition reaction will occur. The result will be a composition containing alkylaluminum groups (in this case, methylaluminum) and functional groups where carbon is also
- 20 bound to oxygen (in this case, a 1,1-diphenyl-ethoxy functional group):

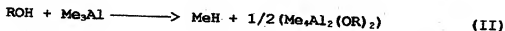
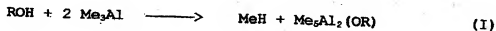


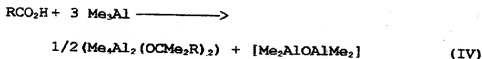
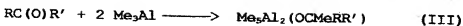
- 25 Analogous precursor compositions can be formed in alternative ways, as will be described in more detail below. As another example, a salt metathesis reaction can be depicted as follows:



As earlier mentioned, the precursor intermediate composition can be formed by using a reagent, containing a carbon-to-oxygen chemical bond. Suitable reagents which can be used can be selected from the alcohols, the ketones, and the carboxylic acids as representative examples. A particularly suitable inorganic reagent which has been found to work is carbon dioxide.

In the preferred embodiment of the present invention, this precursor composition is formed by treating trimethylaluminum with an oxygenated organic compound such as an alcohol, ketone, carboxylic acid or carbon dioxide. In the case of carboxylic acids or carbon dioxide, some aluminoxane moieties will form (see, for example, copending application U.S. Serial No. 08/651,290, filed on May 22, 1996). In all these cases, as is well known in the art (see, for instance, the citations to exhaustive methylation given above, and references cited therein), alkoxyaluminum or arylalkoxyaluminum moieties will be formed. The following equations represent possible, non-limiting, examples of the reactions of trimethylaluminum and oxygenated organic molecules to form alkoxyaluminum or arylalkoxyaluminum-based aluminoxane precursor compositions (R and R' being the same or different and being selected from alkyl and/or aryl and TMAL indicating trimethylaluminum):





5

The most preferred embodiment of the present invention is to use a carboxylic acid or carbon dioxide as they form both a methylaluminum precursor containing the alkoxyaluminum or
 10 arylalkoxyaluminum moieties and the desired methylaluminum products.

Once this preferred methylaluminum precursor composition is formed, the key component of the present invention is the thermal and/or catalytic transformation of
 15 this precursor to form the desired catalytically useful methylaluminum composition. While the prior art teaches that these precursor compositions can be transformed to form exhaustively methylated organic derivatives, it does not disclose the formation of catalytically active aluminosilane
 20 compositions, nor does it teach the proper conditions to form such a catalytically useful composition comprising methylaluminum. A recent review in the prior art (Comprehensive Organometallic Chemistry II, Vol. 1, p. 452) suggests, in fact, that polymethylaluminum processes based on carboxylic
 25 acid reagents "do not produce aluminosilanes suitable for catalytic applications". The prior art additionally fails to recognize the aliphatic hydrocarbon solubility and

improved storage stability characteristics of the preferred products of the process of the present invention as well as the possibility of manufacturing the novel low TMAL-containing product of certain embodiments of the
5 instant invention. The prior art appears to be silent on exhaustive methylation of carbon dioxide. Furthermore, as the Examples provided hereinbelow illustrate, we have discovered conditions where this reaction remains homogeneous, in contrast to the heterogeneous examples of
10 the prior art.

The present invention has also discovered that formation of PMAO, for example, by the present invention yields, in certain embodiments, a product substantially free of TMAL since separate signals for PMAO and TMAL are
15 not observed in the ^1H NMR spectrum of the product.

The process of the present invention produces high recoveries of aluminum as compared to hydrolytic processes for making aluminoxanes as conventionally known to the art. The process of the present invention also is capable
20 of producing polymethylaluminoxane with improved storage stability as compared to hydrolytic processes for making aluminoxanes as conventionally known to the art. Finally, the process of this invention is capable of producing polymethylaluminoxane in high yield in the presence of
25 aliphatic solvents, unlike hydrolytic processes for making aluminoxanes as conventionally known in the art.

The preferred method for transforming the methylaluminoxane precursor is to optionally add, or form in situ, a catalytically effective amount of
30 methylaluminoxane with the precursor and heat the material at the lowest temperature sufficient to effect conversion to the desired methylaluminoxane composition in a

reasonable amount of time. This reaction can also be facilitated by increasing the concentration of organometallic species by removing, or limiting in other ways, the amount of solvent, if solvent, which is an optional ingredient at this point in the process, is present.

The present invention, in its most preferred embodiment is a novel process, for forming catalytically useful polymethylaluminoxane with the resulting, polymethylaluminoxane composition, in certain embodiments being a novel polymethylaluminoxane composition which is substantially free of trimethylaluminum. This process comprises the thermal and/or catalytic transformation of an appropriately constituted precursor composition as earlier described. A preferred method for preparing the precursor composition is treatment of trimethylaluminum with a carboxylic acid or with carbon dioxide. However, as will be appreciated by a person of ordinary skill in the art, there are many other methods which can be used to prepare the precursor composition which is transformed into the desired final product.

If desired, supported polyalkylaluminoxane compositions can be prepared by conducting the aforementioned reaction in the presence of a suitable support material. Alternatively, supported alkylaluminoxanes may also be prepared by forming the alkylaluminoxanes of this invention in a discrete, separate step and subsequently allowing the alkylaluminoxane to react with the support material. Oxidic support materials, such as silica, are especially preferred. It is preferred to have the alkylaluminoxane in a suitable, heated solvent at a temperature high enough

(e.g., at least 85°C, preferably about 100°C) so that the alkylaluminumoxane is in soluble form and, after being combined with the support material, will come out of solution and contact that support as the total system is allowed to cool.

It has now discovered that the non-hydrolytic PMAO ("PMAO-IP") of the present invention has surprising advantages over conventional, hydrolytically prepared PMAO in the preparation of the aforementioned supported methylaluminumoxanes ("SMAO"). PCT Patent Publication No. WO 96/16092 describes a supported catalyst component prepared by heating a support material containing aluminumoxane under an inert atmosphere and at a temperature sufficient to fix aluminumoxane to the support material.

In this publication the aluminumoxane and support are first contacted in a diluent or solvent, which is removed prior to the heat treatment step. This disclosure relies upon the use of an aluminumoxane which is prepared by the controlled hydrolysis of trimethylaluminum species. The instant application discloses novel, non-hydrolytic routes to aluminumoxanes, which have not previously been applied to the problem of preparing a supported catalyst component. Surprisingly, in accordance with the present invention, it has been found that the utilization of non-hydrolytic polymethylaluminumoxane (PMAO-IP), instead of conventional, hydrolytic, polymethylaluminumoxane (PMAO), allows for the preparation of a supported aluminumoxane catalyst component with high recovery of aluminum, with low extractable aluminum, with superior ability to bind a transition metal component, and which can be converted to a catalyst with superior polymerization activity. When a corresponding supported aluminumoxane catalyst component is prepared from

conventional, hydrolytically prepared PMAO, poor recoveries of aluminum were observed, and the resulting supported aluminoxane catalyst component had an inferior ability to bind zirconium, for example.

- 5 As will be appreciated by the person of ordinary skill in the art, the aluminoxane products that can be made by the process of the present invention are useful as cocatalysts in those single-site (metallocene-based) catalyst systems which are useful in the polymerization of
- 10 olefin monomers in a manner analogous to that in current use with the aluminoxane compositions that are currently known and used in that manner.

 The present invention will be further illustrated by the Examples which follow.

15

EXAMPLES

- Standard air-free glovebox and Schlenk line techniques were used. Polymerization tests were conducted in hexane at 85 °C, under a total pressure of 150 psig (ethylene + hexane + hydrogen), using rac-ethylenebisindenylzirconium dichloride:trimethylaluminum 1:30 as the catalyst precursor component with the aluminoxane present at 1000:1 Al:Zr. Trimethylaluminum (37.2 wt % Al) and polymethylaluminoxane (PMAO) in toluene (9.0 wt % Al) were obtained from Akzo Nobel Chemicals Inc., Deer Park TX, and used as received. Benzophenone and benzoic acid were obtained from Aldrich Chemical Co., placed under a nitrogen atmosphere, and otherwise used as received.

EXAMPLE 1

A solution of trimethylaluminum (2.00 g trimethylaluminum, 15.6 g toluene) was treated with a solution of benzophenone (4.02 g benzophenone, 15.6 g toluene), and the resulting mixture heated at 60 °C for one and one half hours to give a solution of alkylaluminum arylalkoxides with the overall composition $((C_6H_5)_2MeCO)_0.8AlMe_{2.2}$. Analysis of this product by 1H NMR showed it to be a mixture of the discrete compounds: $((C_6H_5)_2MeCO)_1AlMe_2$ and $((C_6H_5)_2MeCO)_1Al_2Me_5$. This product could be heated, as is, for many hours at 60 °C and remain unchanged according to 1H NMR.

A catalytic amount of PMAO (0.35 g, 9.0 wt % Al) was added to the alkylaluminum arylalkoxide solution, and the mixture heated at 60 °C for 3.2 hours. At the end of this time, analysis by 1H NMR showed that alkoxy aluminum species were no longer present, and that aluminoxane moieties were present. An ethylene polymerization test, which normally yields about 700 kg PE/g Zr hr with conventional PMAO prepared by Akzo Nobel Chemicals Inc., gave 1380 kg PE/g Zr hr using this polymethylaluminoxane instead.

EXAMPLE 3

5 TMAL (15.00 g) was mixed with toluene (9.25 g) and
was then reacted with carbon dioxide (3.74 g) at room
temperature to form an alkoxyaluminum and
alkylaluminum-oxane-containing PMAO precursor composition.
This mixture was heated at 100° C for twenty-four hours to
give a clear, viscous liquid whose ¹H NMR showed it to have
10 been converted to PMAO. Alkoxyaluminum species were no
longer detectable by NMR analysis. As no insoluble
aluminum-containing byproducts were formed, this
preparation gave a quantitative yield of catalytically
useful polymethylaluminum-oxane. A polymerization test with
15 this material yielded 2400 kg PE/g Zr hr in a thirty
minute test.

EXAMPLE 4

5 Using the same procedure that is described in Example
2, TMAL (8.00 g) in 9.51 g of toluene was treated with
neat benzoic acid (5.40 g) to give an arylalkoxyaluminum-
containing methylaluminumoxane precursor. Heating of this
mixture at 80°C for five hours gave conversion to PMAO. As
10 no insoluble aluminum-containing byproducts were formed,
this preparation gave a quantitative yield of
catalytically useful polymethylaluminumoxane.

Fig. 1 shows the Me-Al region of a ^1H NMR spectrum of
conventional PMAO obtained from a commercial source. The
15 spectrum clearly contains two signals, a broad signal due
to methylaluminumoxane species, and a sharper signal due to
trimethylaluminum species. Fig. 2 shows the same region
of the spectrum of PMAO prepared in this Example. Unlike
the commercially available PMAO, the material of this
20 invention shows only one broad signal in the depicted
region. The product is substantially free of TMAL in that
no distinct ^1H NMR signal from TMAL is discernible.

EXAMPLE 5

- 5 A solution of trimethylaluminum (8.0 g in 4.94 g of decane) was treated with carbon dioxide (1.9 g of carbon dioxide) over a period of eight hours. Analysis by ^1H NMR showed this mixture to contain $(\text{CH}_3)_3\text{CO-Al}$, $\text{CH}_3\text{-Al}$, and Al-O-Al moieties. Heating this sample at 100°C for twenty-
- 10 four hours caused no change in the ^1H NMR spectrum. However, when heated for five hours at 120°C , the reaction mixture became slightly hazy, forming a viscous liquid after cooling. Since it was not necessary to separate solid, aluminum-containing byproducts from this product,
- 15 this preparation gave a quantitative yield of catalytically useful polymethylaluminoxane. Analysis by ^1H NMR showed signals due to decane solvent, traces of residual t-butoxy signals, and a broad signal due to methylaluminoxane species.
- 20 An ethylene polymerization test gave 1100 kg PE/g Zr/hr using the polymethylaluminoxane prepared in this Example.

EXAMPLES 6-15

All manipulations in these Examples were conducted with the best available air-free techniques, including
5 Schlenk line manipulations and inert atmosphere glove-box techniques. On-line monitoring of the box atmosphere generally showed 0.1-1.5 ppm oxygen (with brief excursions to 2-6 ppm when opening the ante-chamber door) and 0.5-3 ppm water (with excursions to about 6 ppm).

- 10 Polymerization tests were conducted in a jacketed one liter stainless steel ZIPPERCLAVE autoclave from Autoclave Engineers. The polymerization reactions were conducted with 150 psig ethylene supplied on demand to a reactor charged with 25-50 mg of the catalyst (containing 1-2
15 micromoles Zr, depending on expected activity and planned test duration), 500 mL hexane, and 2 mmole TEAL (present as a scavenger). Prior to each polymerization test, the reactor body was removed and oven dried for one hour at 100°C-120°C (with water drained from the heating/cooling
20 jacket). The reactor was always reassembled while the body was still hot from the oven, and purged with nitrogen for 15-30 minutes while the reactor cooled somewhat. After purging, the recirculating bath was reconnected, and the reactor heated to 50°C. The reactor was pre-treated
25 with TEAL (0.2 mmole) in hexane (300 mL).

Prior to use, DAVISON 948 micro-spherical silica was dehydrated by calcination in a nitrogen fluidized bed. Table 1 summarizes silica used in this work.

- 30 Non-hydrolytically prepared polymethylaluminoxane (PMAO-IP) was prepared according to the general teachings of Example 3 contained herein.

Table 1. Calcination results.

	Calcination Temp. °C	wt. loss (%)	Residual OH mmole/g
Silica A	200 °C	3.9	1.52
Silica B	400 °C	6.2	1.06
Silica C	400 °C	5.5	1.06
Silica D	600 °C	7.1	0.65
Silica E	600 °C	6.2	0.71

5 General Procedure for Making SMAO: This is the
procedure used for all the samples in Tables 2 and 3. A
three-neck glass reactor (250 mL), equipped with gas
inlet, fritted-glass barrier gas-outlet, temperature
10 sensor and overhead stirrer (crescent-shaped paddle) was
placed under a nitrogen atmosphere and charged with 10.11
g silica (Silica D). Toluene (45 g) was added to form a
slurry, and stirring was begun. An aliquot of PMAO-IP
solution (14.91 g, 14.8 wt % Al) was then added, dropwise,
15 over 0.5 hour with stirring at 23-24°C. After the addition
was completed, the reaction mixture was heated to 100°C in
order to insure solubilization of the PMAO-IP, and was held
at that temperature for one hour. After the reaction
mixture had cooled back to room temperature, it was
20 transferred via a 1/4 inch outer diameter polyethylene
tube cannula to a bottom-fritted three-neck glass reactor
(250 mL), equipped with gas inlet, fritted-glass barrier
gas-outlet, and temperature sensor. The supernate was
removed, and the SMAO product was isolated by filtration
25 through the bottom frit. The filtrate was collected and
was set aside for analysis. The SMAO was then vacuum
dried in a bath at 50°C to obtain a free-flowing powder.
The results are summarized in Tables 2 and 3 which follow:

Table 2. Summary of SMAO preparation data.

	SiO ₂	SiO ₂	PMAO	PMAO	Toluene	SMAO	SMAO
		(g)	(wt % Al)	(wt % Al)	(total g)	(g)	(wt % Al)
Comp. Ex. A	Silica B	5.0	Conventional	9.0	80.2	5.5	9.7
Example 6	Silica A	10.0	PMAO-IP	14.8	89.41	13.2	12.2
Example 7	Silica C	20.0	PMAO-IP	15.1	186.7	20.97	11.4
Example 8	Silica D	10.0	PMAO-IP	14.8	90.2	12.83	12.3
Example 9	Silica E	10.0	PMAO-IP	13.3	88.2	14.1	14.1
Example 10	Silica E	100	PMAO-IP	13.3	801	144	13.3

Table 3. Summary of SMAO preparations.

Sample	Al:SiO ₂ (g/g)	Al (wt %)	% Al as SMAO	Solution Al ³⁺ wt %	% Al soluble ⁴
Comp. Ex. A	0.18	9.7	60	0.43	18
Example 6	0.18	12.2	91	0.13	8
Example 7	0.18	11.4	88 ⁵	0.28	6
Example 8	0.18	12.3	88	<0.01	0
Example 9	0.22	14.1	90	<0.01	0
Example 10	0.22	13.3	87	<0.01	0

¹ Grams of aluminum charged divided by grams of dehydrated silica charged.

² Fraction of aluminum recovered in the SMAO, expressed as percent.

³ Concentration of aluminum in supernate decanted or filtered from the SMAO preparation.

⁴ Fraction of aluminum recovered in the filtrate or decant, expressed as percent.

⁵ There was some unusual handling loss in this sample.

Conversion to catalyst:

The SMAO samples in Table 3 were converted to single-site based ethylene polymerization catalysts by allowing up to 1 Zr:100 Al to bind with the SMAO from a solution of a bis-indenyl dimethylzirconium (BIZ-M) in toluene. A 250 mL catalyst preparation flask (3 neck flask with bottom frit), with an ace-threaded gas inlet adapter containing a thermocouple, a stopper, and a fritted gas adapter, was set up and was tested for vacuum. Working in the glovebox, the apparatus was charged with 5 grams of the selected SMAO sample, and the central stopper was replaced with an overhead stirring shaft. At the same time, one 10 g, and three 15 gram charges of dry toluene were set up in serum-capped sample vials. Also prepared at this time was a 50 mL septum bottle with BIZ-M (usually about 100 mg) and a small stir bar. Enough toluene (typically 30 g) was added to obtain complete dissolution.

Working on a Schlenk line, the first 10 g charge of toluene was used to slurry the silica. Gentle stirring was then begun. Enough BIZ-M solution to provide 1 Zr:100 Al in the SMAO sample was then added, and the mixture was heated to 50°C for one hour and was then filtered. The catalyst was then washed with two of the 15 g toluene charges. All the filtrates were combined.

The stirrer was replaced with a stopper, and the catalyst was vacuum dried at room temperature until "fountaining" of catalyst (due to out-gassing of solvent vapors) was no longer observed (generally less than thirty minutes). After this, the catalyst was dried for an additional thirty minutes at room temperature, and then thirty more minutes at 35 °C. Tables 4-6 which follow gives a summary of the catalyst preparations and performance data:

Table 4 Summary of Catalyst Preparations.⁶

SMAO	Catalysts	Al ⁷	Al ⁸	Sol. Al ⁹	Zr ¹⁰	Zr ¹¹	Sol. Zr ¹²	Al/Zr	D10	D50	D90
Sample	Sample	wt %	Rcvry	wt %	wt %	Rcvry	ppm	ratio	(microns)		
Comp A	Comp B	8.3	81	0.13	0.21	47	74	133	15	56	83
Ex. 6	Ex. 11	11.9	96	0.03	0.39	90	< 8	103	25	51	76
Ex. 7	Ex. 12	11.4	74	<0.01	0.38	96	< 8	101	30	53	80
Ex. 8	Ex. 13	11.9	88	<0.01	0.40	96	< 8	101	20	49	73
Ex. 9	Ex. 14	13.9	93	<0.01	0.43	85	<8	109	22	48	72
Ex. 10	Ex. 15	13.3	95	<0.01	0.44	92	<8	102	17	51	79

⁶ Use Table 3 as a 'key' to the samples in this and subsequent tables.⁷ Concentration of aluminum in the isolated catalyst.⁸ Fraction of aluminum recovered in the isolated catalyst, expressed as percent.⁹ Concentration of aluminum in supernate decanted or filtered from the catalyst preparation.¹⁰ Concentration of zirconium in the isolated catalyst.¹¹ Fraction of zirconium recovered in the isolated catalyst, expressed as percent.¹² Concentration of aluminum in supernate decanted or filtered from the catalyst preparation.

5

Table 6. Summary of performance results.

SMAO Sample	Cat. Sample	Activity kg PE/g hr	D10	D50 (microns)	D90	PBD g/mL
Comp A	Comp B	0.5	—	—	—	0.39
Ex. 6	Ex. 11	0.6	306	388	468	0.32
Ex. 7	Ex. 12	0.7	—	—	—	0.34
Ex. 8	Ex. 13	0.65	—	—	—	0.34
Ex. 9	Ex. 14	1.6	432	507	573	0.36
Ex. 10	Ex. 15	1.3	392	451	492	0.36

10 The data show above shows that PMAO-IP binds more completely to calcined silica than conventional PMAO-IP, allows for the preparation of SMAO with a higher aluminum loading, and results in SMAO that binds more completely to zirconium species thereby forming a more active catalyst.

15

The foregoing Examples, since they merely illustrate certain embodiments of the present invention, should not be construed in a limiting sense. The scope of protection sought is set forth in the claims which follow.

We Claim:

1. A polymethylaluminum composition substantially free of trimethylaluminum.
2. A process which comprises the non-hydrolytic transformation of an aluminosilicate precursor composition, which comprises moieties containing carbon-to-oxygen bonds that can be alkylated by alkylaluminum moieties, to form a composition comprising catalytically useful alkylaluminosilicate moieties.
3. The process of Claim 2 where the aluminosilicate precursor composition is formed by the reaction of a trialkylaluminum compound, or a mixture of trialkylaluminum compounds, and a compound containing carbon-to-oxygen bonds.
4. The process of Claim 2 where the aluminosilicate precursor composition is formed by the reaction of a trialkylaluminum compound, or a mixture of trialkylaluminum compounds, and carbon dioxide.
5. The process of Claim 3 wherein the compound is selected from the group consisting of the alcohols, ketones, and the carboxylic acids.
6. The process of Claim 2 wherein the precursor composition is thermally transformed and had been formed by the reaction of a

trialkylaluminum compound, or a mixture of trialkylaluminum compounds, and carbon dioxide.

7. The process of Claim 6 where the mixture of trialkylaluminum compounds comprises trimethylaluminum and one or more trialkylaluminum compounds comprising an alkyl group which comprises two or more carbon atoms.

8. The product formed by the process of any of Claims 2 to 7.

9. A polymethylaluminoxane product formed by the process of any of Claims 2 to 7.

10. The supported product formed by the process of any of Claims 2 to 7.

11. The supported polymethylaluminoxane product formed by the process of any of Claims 2 to 7.

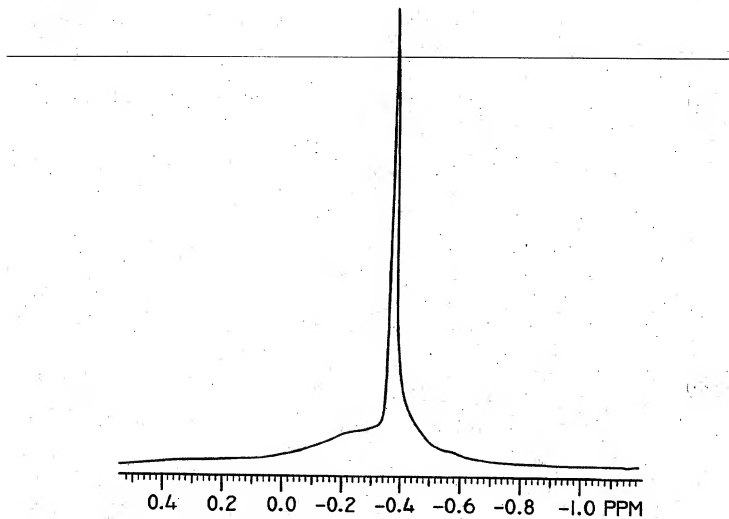
12. The silica-supported polymethylaluminoxane product formed by the process of any of Claims 2 to 7.

13. Catalyst compositions for use in the polymerization of olefins which comprise the aluminoxane, optionally on a support, formed by the process of any of Claims 2 to 7.

14. Catalyst compositions for use in the polymerization of olefins which comprise a polymethylaluminoxane, optionally on a support, formed by the process of any of Claims 2 to 7.

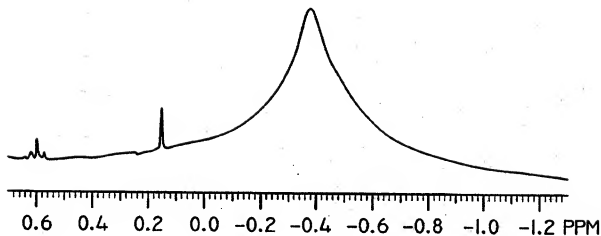
1/2

FIG. 1



2/2

FIG. 2



SUBSTITUTE SHEET (RULE 26)

INTERNATIONAL SEARCH REPORT

International application No.

PCT/US96/19980

A. CLASSIFICATION OF SUBJECT MATTER

IPC(6) :B01J 31/00, 37/02; C07F 5/06; C08F 4/44

US CL :502/103, 117, 152; 526/160, 943; 556/175, 179, 182, 190

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

U.S. : 502/103, 117, 152; 526/160, 943; 556/175, 179, 182, 190

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)

APS, CAS ONLINE

search term: polymethylaluminoxane(s)

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	US 5,235,081 A (SANGOKOYA) 10 August 1993, see Tables 1-3 and claims 14-17.	1, 8 and 9
Y		10-14
A	US 4,544,762 A (KAMINSKY et al.) 01 October 1985, see entire document.	1-14
A	JP 405059068 A (TOSOH AKZO CORP) 09 March 1993, see entire document.	1-14
A	WO 89/02453 A1 (THE DOW CHEMICAL COMPANY) 23 March 1989, see entire document.	1-14

☐ Further documents are listed in the continuation of Box C.
 ☐ See patent family annex.

* Special categories of cited documents:	"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention
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"P" document published prior to the international filing date but later than the priority date claimed	

Date of the actual completion of the international search	Date of mailing of the international search report
19 MARCH 1997	04 APR 1997
Name and mailing address of the ISA/US Commissioner of Patents and Trademarks Box PCT Washington, D.C. 20231	Authorized officer Porfirio Nazario-Gonzalez
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